



Designation: **D 4328 – 9703**

Standard Practice for Calculation of Supersaturation of Barium Sulfate, Strontium Sulfate, and Calcium Sulfate Dihydrate (Gypsum) in Brackish Water, Seawater, and Brines¹

This standard is issued under the fixed designation D 4328; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon (ϵ) indicates an editorial change since the last revision or reapproval.

1. Scope

1.1 This practice covers the calculation of supersaturation of barium sulfate, strontium sulfate, and calcium sulfate dihydrate (gypsum) in brackish water, seawater, and brines in which barium, strontium, and calcium ions either coexist or exist individually in solution in the presence of sulfate ions.

1.2 This practice is not applicable for calculating calcium sulfate dihydrate supersaturation if the temperatures of saline waters under investigation exceed 95°C. At temperatures above 95°C, hemianhydrate and anhydrite would be major insoluble forms.

1.3 *This standard does not purport to address all of the safety concerns, if any, associated with its use. It is the responsibility of the user of this standard to establish appropriate safety and health practices and determine the applicability of regulatory limitations prior to use.*

2. Referenced Documents

2.1 ASTM Standards:

¹ This practice is under the jurisdiction of ASTM Committee D-19 on Water and is the direct responsibility of Subcommittee D19.05 on Inorganic Constituents in Water. Current edition approved Dec. 10, 1997; 2003. Published December 1998; January 2003. Originally published as D 4328-84, approved in 1984. Last previous edition approved in 1997 as D 4328-84 (1993)¹; 4328-97.

- D 511 Test Methods for Calcium and Magnesium in Water²
- D 512 Test Methods for Chloride Ion in Water
- D 513 Test Methods for Total and Dissolved Carbon Dioxide in Water²
- D 516 Test Method for Sulfate Ion in Water²
- D 1129 Terminology Relating to Water²
- D 1192 Specification for Equipment for Sampling Water and Steam in Closed Conduits²
- D 3352 Test Method for Strontium Ion in Brackish Water, Seawater, and Brines³
- D 3370 Practices for Sampling Water from Closed Conduits²
- D 3561 Test Method for Lithium, Potassium, and Sodium Ions in Brackish Water, Seawater, and Brines by Atomic Absorption Spectrophotometry³
- D 3651 Test Method for Barium in Brackish Water, Seawater, and Brines³
- D 3986 Test Method for Barium in Brines, Seawater, and Brackish Water by Direct-Current Argon Plasma Atomic Emission Spectroscopy³

3. Terminology

3.1 *Definitions:* For definitions of terms used in this practice, refer to Terminology D 1129.

4. Significance and Use

4.1 This practice covers the mathematical calculation of the supersaturation of three principal sulfate scaling compounds found in industrial operations. Application of this standard practice to the prediction of scale formation in a given system, however, requires experience. The calculations tell the user if a water, or mixture of waters, is in a scaling mode. Whether or not scale will in fact form, how quickly it will form, where it will form, in what quantities, and what composition are subject to factors beyond the scope of this practice. However, based on how supersaturated a given water or mixture of waters is, an objective evaluation of the relative likelihood of scale formation can be made.

NOTE 1—There are several personal computer (PC) type programs that are both available commercially and publicly that will perform these calculations.

5. Procedure

- 5.1 Collect water samples for compositional analysis in accordance with Practices D 3370 and Specification D 1192.
- 5.2 Determine the calcium and magnesium concentrations in accordance with Test Methods D 511.
- 5.3 Determine the barium concentration in accordance with Test Methods D 3651 or D 3986.
- 5.4 Determine the strontium concentration in accordance with Test Method D 3352.
- 5.5 Determine sodium and potassium concentrations in accordance with Test Method D 3561.
- 5.6 Determine sulfate ion concentration in accordance with Test Method D 516.
- 5.7 Determine chloride ion concentration in accordance with Test Methods D 512.
- 5.8 Determine carbonate and bicarbonate ion concentrations in accordance with Test Methods D 513.
- 5.9 Determine the concentrations of all other major inorganic constituents that may be present in the water under investigation in accordance with appropriate test methods in *Annual Book of ASTM Standards*, Vols 11.01 and 11.02.
- 5.10 Determine temperature and pressure of the water system under investigation.

6. Calculation of Ionic Strength

6.1 Calculate the ionic strength of the water under investigation as follows:

$$\mu = \frac{1}{2} \sum C_i Z_i^2 \quad (1)$$

where:

- μ = ionic strength,
- C_i = molal concentration of each ion in solution, and
- Z_i = charge number of ion, i.

7. Calculation of Barium Sulfate Supersaturation (Refer to Appendix X1)

7.1 Calculate barium sulfate solubility in the water under investigation, using the equation as follows:

$$S = (\sqrt{X^2 + 4K} - X)/2 \quad (2)$$

where:

² *Annual Book of ASTM Standards*, Vol 11.01.

³ *Annual Book of ASTM Standards*, Vol 11.02.

S = solubility, moles of solute per kilogram of water corrected for the common ion effect,
 K = solubility product constant (molal) at the ionic strength, temperature and pressure of the water under investigation. For BaSO_4 refer to Appendix X2, and
 X = molal excess of soluble common ion.

7.2 Calculate the amount of barium sulfate, moles per kilogram of water, in the sample based on the lesser of the barium or sulfate ion concentration.

7.3 If the amount of BaSO_4 in the sample (7.2) is less than its calculated solubility (7.1), the water in question is undersaturated with respect to BaSO_4 . If the amount of BaSO_4 present is greater than its solubility, the water is supersaturated with respect to BaSO_4 . Calculate the amount of supersaturation as the difference between the two values:

$$\text{supersaturation} = \text{concentration} - \text{solubility} \quad (3)$$

NOTE 2—Supersaturation may also be calculated directly from the equation (1)⁴

$$([\text{Ba}^{++}] - y)([\text{SO}_4^{=}] - y) = K \quad (4)$$

where:

Ba^{++} = concentration of barium, molal,

$\text{SO}_4^{=}$ = concentration of sulfate, molal,

y = excess (supersaturation) of BaSO_4 , molal, and

K = solubility product constant (molal) of BaSO_4 at test conditions.

The value X may then be determined from the quadratic equation (see Appendix X1):

$$X = \frac{-B \pm \sqrt{B^2 - 4AC}}{2A}$$

Report BaSO_4 supersaturation in molal terms of the weight of BaSO_4 per volume of water, mg/L.

$$\begin{aligned} & \text{BaSO}_4 \text{ supersaturation, mg/L} \\ &= \text{BaSO}_4, (\text{molal}^2) \times 10^3 \times 233 \times \left(\frac{1000 \times D}{TDS} + 1000 \right) \end{aligned}$$

where D = sample density.

8. Calculation of Strontium Sulfate Supersaturation (Refer to Appendix X1)

8.1 Calculate strontium sulfate solubility using the same steps described for BaSO_4 (Section 7), but substituting the appropriate values for SrSO_4 in Eq 2 (Refer to Appendix X3 or Appendix X4).

NOTE 3—If barium sulfate supersaturation exists, the amount of sulfate available for strontium sulfate will be less by the amount of sulfate equivalent to the calculated BaSO_4 supersaturation.

NOTE 4—If carbonate ions are present, strontium carbonate may precipitate. The amount of strontium may then be corrected by that required for strontium carbonate precipitation prior to the calculation of SrSO_4 solubility. (6) Practically speaking, however, due to the extremely low solubility of SrCO_3 , this correction may usually be omitted.

8.2 Calculate the amount of strontium sulfate moles per kilogram water in the sample based on the lesser of the strontium or remaining sulfate ion concentration.

8.3 If the amount of SrSO_4 in the sample (8.2) is less than its calculated solubility (8.1), the water in question is undersaturated with respect to SrSO_4 . If the amount of SrSO_4 present is greater than its solubility, the water is supersaturated with respect to SrSO_4 . Calculate the amount of supersaturation, moles per kilogram water by difference (Eq 3), or by substituting appropriate data in Eq 4 (Note 2).

8.3.1 Report SrSO_4 supersaturation in terms of the weight of SrSO_4 per volume of water as follows:

$$\begin{aligned} & \text{SrSO}_4 \text{ supersaturation mg/L} \\ &= \text{SrSO}_4, (\text{molal}) \times 10^3 \times 184 \times \left(\frac{1000 \times D}{TDS} + 1000 \right) \end{aligned}$$

9. Calculation of Calcium Sulfate Supersaturation (Refer to Appendix X1)

9.1 Calculate calcium sulfate solubility using the same steps described for BaSO_4 (Section 7), but substituting the appropriate values for CaSO_4 in Eq 2 (Refer to Appendix X5).

9.2 Calculate the amount of calcium sulfate moles per kilogram in the sample based on the lesser of the calcium or remaining sulfate ion.

⁴ The boldfaced numbers in parentheses refer to a list of references at the end of this standard.

9.3 If the amount of CaSO_4 in the sample (9.2) is less than its calculated solubility (9.1), the water in question is undersaturated with respect to CaSO_4 . If the amount of CaSO_4 present is greater than its solubility, the water is supersaturated with respect to CaSO_4 . Calculate the amount of supersaturation moles per kilogram by difference (Eq 3) or by substituting appropriate data in Eq 4 (Note 2).

9.3.1 Report CaSO_4 supersaturation in terms of the weight of $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$ (gypsum) per volume of water after converting moles per data obtained above to mg/L as follows:

$$\begin{aligned} & \text{CaSO}_4 \cdot 2\text{H}_2\text{O} \text{ supersaturation, mg/L} \\ & = \text{CaSO}_4 \cdot 2\text{H}_2\text{O}_2, \text{ moles/kg} \times 172.17 \times 10^3 \times D \end{aligned}$$

10. Keywords

10.1 barium sulfate; brines; calcium sulfate dihydrate; strontium sulfate

APPENDIXES

(Nonmandatory Information)

X1. SAMPLE CALCULATION OF BaSO_4 SUPERSATURATION AT 95°C

Analysis of Water				Ionic Strength	
Component Ions	mg/L	moles per litre ^A	molal ^A Concentration	Z ²	$\mu = \frac{1}{2} \sum Z_i^2$ (Section 6)
Na	27 120	1.180	1.214	1	1.214
Ca	10 890	0.272	0.280	4	1.120
Mg	1679	0.69	0.071	4	0.284
Ba	6.4	0.000044	4.52×10^{-5}	4	>0.001
Sr	444	0.00506	521.42×10^{-5}	4	0.021
Cl	64 870	1.830	1.883	1	1.883
SO ₄	1210	0.012596	1296.14×10^{-5}	4	0.052
HCO ₃	317	0.005	0.005	1	0.005
TDS = 106 536				Total ionic strength = 2.29	
Density = 1.078 g/ml				K_{BaSO_4} at 95° (Appendix X1) = 83.22×10^{-9}	

^A

$$\begin{aligned} \text{Convert moles/L to molal} &= \text{moles/L} \times \frac{1000}{(\text{Sp gr} \times 1000) - \frac{\text{TDS}}{1000}} \\ &= \text{moles/L} \times \frac{1000}{1078 - 106.5} \\ &= \text{moles/L} \times 1.029 \end{aligned}$$

X1.1 BaSO_4 solubility (refer to 7.1)

$$S = (\sqrt{X^2 + 4K} - X)/2$$

where:

X = molal excess of common ion (in this case SO_4),

$$\begin{aligned} X &= (1296.14 \times 10^{-5}) - (4.52 \times 10^{-5}) \\ &= 1291.62 \times 10^{-5} \end{aligned}$$

$$4K = 4(83.22 \times 10^{-9}) = 332.88 \times 10^{-9}, \text{ or } 3328.8 \times 10^{-10}$$

$$S = \left[\frac{\sqrt{(1291.62 \times 10^{-5})^2 + (3328.8 \times 10^{-10})} - (1291.62 \times 10^{-5})}{2} \right]$$

$$\text{Solubility } S = 0.644 \times 10^{-5} \text{ molal}$$

X1.2 BaSO_4 present (refer to 7.2):

X1.2.1 Ba present = 4.52×10^{-5} molal

X1.2.2 SO_4 present = 1296.14×10^{-5} molal

X1.2.3 Based on lower value (Ba), BaSO_4 present = 4.52×10^{-5} molal

X1.3 Amount of BaSO_4 supersaturation (refer to 7.3)

X1.3.1 BaSO_4 present based on $\text{Ba}^{++2+} = 4.52 \times 10^{-5}$ molal

X1.3.2 Calculated BaSO_4 solubility, $S = 0.64 \times 10^{-5}$ molal

X1.3.3 BaSO_4 excess; i.e. supersaturation = 3.88×10^{-5} molal; or 8.8 mg/L of sample

X1.4 *Useful Information :*

	Mol Weight	Equivalent Weight	Gravimetric Conversion Factors
Ba	137.33	68.66	$\text{Ba} \times 1.6995 = \text{BaSO}_4$
Ca	40.08	20.04	$\text{Ca} \times 3.3967 = \text{CaSO}_4$
Sr	87.62	43.81	$\text{Sr} \times 2.0963 = \text{SrSO}_4$
SO_4	96.06	48.03	
BaSO_4	233.39	116.70	$\text{SO}_4 \times 2.4296 = \text{BaSO}_4$
CaSO_4	136.14	68.07	$\text{SO}_4 \times 1.4172 = \text{CaSO}_4$
$\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$	172.14	86.07	$\text{SO}_4 \times 1.9121 = \text{SrSO}_4$
SrSO_4	183.68	91.84	

X1.5 The amount of supersaturation (excess BaSO_4) may also be calculated directly using the expression (Eq 4):

$$([\text{Ba}^{++}] - X) ([\text{SO}_4] - X) = K_{\text{BaSO}_4}$$

X1.5.1 Using the molal values from the water analysis above this becomes:

$$([4.52 \times 10^{-5}] - X) ([1296.14 \times 10^{-5}] - X) = 832.2 \times 10^{-10}$$

$$\text{Multiplying: } (5858.55 \times 10^{-10}) - (1300.66 \times 10^{-5})$$

$$X + X^2 = 832.2 \times 10^{-10}$$

$$\text{Combining: } X^2 - (1300.66 \times 10^{-5})X + 5026.35 \times 10^{-10} = 0$$

X1.5.2 Substituting the above coefficients of X in the quadratic equation:

$$X = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a}$$

and solving, $X = 3.88 \times 10^{-5}$ molal; or 8.8 mg/L of sample.

X2. SOLUBILITY DATA FOR $\text{BaSO}_4 \cdot \text{NaCl} \cdot \text{H}_2\text{O}$ SYSTEMS (2)

Solution Ionic Strength, μ	Solubility Product Constant, K (Molal)					
	25°C	35°C	50°C	65°C	80°C	95°C
0.1	1.54×10^{-9}	2.00×10^{-9}	2.70×10^{-9}	3.34×10^{-9}	3.76×10^{-9}	3.97×10^{-9}
0.2	2.70	3.36	4.76	5.93	7.06	7.74
0.4	4.49	5.63	7.92	10.61	13.69	16.13
0.6	6.08	7.74	11.03	15.38	20.45	24.97
0.8	7.74	9.60	13.69	20.16	26.57	33.49
1.0	9.22	11.24	16.38	24.02	32.76	42.02
1.5	12.54	15.38	22.20	32.40	44.94	62.00
2.0	15.63	19.04	27.23	39.60	56.17	78.96
2.5	18.23	21.90	31.33	44.94	63.50	93.64
3.0	20.74	24.65	34.97	49.73	70.23	107.57
3.5	23.41	27.56	38.81	53.82	76.73	120.41
4.0	25.92	30.63	42.44	58.08	82.94	132.50
4.5	28.56	34.23	45.80	63.00	89.40	144.40

X3. SOLUBILITY PRODUCT DATA FOR $\text{SrSO}_4 \cdot \text{NaCl} \cdot \text{H}_2\text{O}$ SYSTEMS (3)

Solution Ionic ^A Strength, μ	Solubility Product Constant, K (Molal)	
	40°C (104°F)	71°C (160°F)
0.1	0.250×10^{-5}	0.160×10^{-5}
0.2	0.390	0.250
0.3	0.505	0.345
0.4	0.617	0.440
0.5	0.723	0.518
0.75	1.02	0.785

Solution Ionic ^A Strength, μ	Solubility Product Constant, <i>K</i> (Molal)	
	40°C (104°F)	71°C (160°F)
1.0	1.26	1.04
1.25	1.48	1.25
1.5	1.68	1.41
1.75	1.86	1.57
2.0	2.00	1.68
2.25	2.09	1.76
2.5	2.14	1.81
2.75	2.16	1.84
3.0	2.17	1.86
3.25	2.19	1.87
3.50	2.20	1.88

^A The above table may be used to interpolate the solubility product (*K*) for SrSO₄ in brines at 0 psig. The interpolated values can be substituted in Eq 2 (Section 6) for estimating the solubility (*S*) of SrSO₄. For more precise *K* values at temperatures up to 300°F (149°C) and pressures up to 3000 psig add SI unit, refer to Appendix X4.

X4. Equation for Calculating SrSO₄ Solubility (4)

X4.1 Experimental SrSO₄ solubility data have been reduced to the following regression equation for calculating the solubility product constant (*K*) at various solution ionic strengths over a temperature range of 100 to 300°F (38 to 149°C) and pressures up to 3000 psig. The equation is adaptable to computer calculation which can then substitute the value for *K* in Eq 2 (Section 6) for computing the solubility of SrSO₄ at desired conditions.

$$\text{Log } K_{\text{SrSO}_4} = X/R$$

where:

$$X = 1/T,$$

$$R = A + BX + C\mu^{1/2} + D\mu + EZ^2 + FXZ + G\mu^{1/2}Z,$$

Z = pressure (psig),

μ = solution ionic strength,

T = temperature, ° K.

X4.1.1 Coefficients of the above equation for *R* are as follows:

$$A = 0.266948 \times 10^{-3}$$

$$B = -244.828 \times 10^{-3}$$

$$C = -0.191065 \times 10^{-3}$$

$$D = 53.543 \times 10^{-6}$$

$$E = -1.383 \times 10^{-12}$$

$$F = 1.103323 \times 10^{-6}$$

$$G = -0.509 \times 10^{-9}$$

X5. SOLUBILITY PRODUCT DATA FOR CaSO₄·NaCl·H₂O SYSTEMS (5)

Solution Ionic Strength, μ	Solubility Product Constant, <i>K</i> (Molal)			
	10°C	35°C	50°C	80°C
0	1.02×10^{-4}	1.27×10^{-4}	1.25×10^{-4}	0.89×10^{-4}
0.1	3.04	3.29	3.31	2.82
0.2	4.99	5.23	5.28	4.67
0.3	6.87	7.11	7.17	6.44
0.4	8.68	8.91	8.96	8.13
0.5	10.41	10.64	10.68	9.75
0.6	12.07	12.30	12.30	11.30
0.7	13.65	13.88	13.85	12.78
0.8	15.16	15.39	15.32	14.18
0.9	16.60	16.83	16.71	15.52
1.0	17.96	18.20	18.02	16.79
1.25	21.05	21.29	20.96	19.70
1.5	23.69	23.93	23.46	22.22
1.75	25.90	26.12	25.52	24.39
2.0	26.67	27.88	27.18	26.22
2.25	29.03	29.22	28.47	27.73
2.5	30.00	30.15	29.40	28.92
2.75	30.60	30.71	30.01	29.81
3.0	30.84	30.90	30.32	30.42
3.25	30.77	30.77	30.36	30.73
3.5	30.39	30.34	30.15	30.76
3.75	29.76	29.66	29.73	30.51
4.0	28.90	28.75	29.13	29.97
4.25	27.85	27.66	28.37	29.14
4.5	26.65	26.43	27.49	28.02
4.75	25.34	25.13	26.52	26.58
5.0	23.98	23.80	25.48	24.83

REFERENCES

- (1) Ostroff, A. G., "Introduction To Oilfield Water Technology," a NACE publication, second edition, 1979.
- (2) Templeton, C. C., "Solubility of Barium Sulfate In Sodium Chloride Solution From 25°C to 95°C," *J. Chem. and Engineering Data*, 5 No. 4, Oct. 1960, p. 514.
- (3) Goldberg, J. B., Jacques, D. F., and Whiteside, W. C., SPE 8874, "Strontium Sulfate Solubility and the Effects of Scale Inhibitors," presented at NACE Middle East Oil Technical Conference/79, Bahrain, March 9–12, 1979.
- (4) Bourland, B. I., and Jacques, D. F. SPE 9625, "A Study of Solubility of Strontium Sulfate," presented at NACE Middle East Oil Technical Conference and Exhibition, Bahrain, March 1981.
- (5) McDonald, Jr., J. P., Skillman, H. L., and Stiff, Jr., H. A., Paper No. 906-14-I, "A Simple Accurate, Fast Method For Calculating Calcium Sulfate Solubility In Oilfield Brine," presented at the Spring Meeting of the South Western District, API, Lubbock, TX, 1969.
- (6) Fletcher, G. E., French, T. R., and Collins, A. G., "A Method for Calculating Strontium Sulfate Solubility, U.S. Department of Energy Publication DOE/BETC/BI-80/10, April 1981.

ASTM International takes no position respecting the validity of any patent rights asserted in connection with any item mentioned in this standard. Users of this standard are expressly advised that determination of the validity of any such patent rights, and the risk of infringement of such rights, are entirely their own responsibility.

This standard is subject to revision at any time by the responsible technical committee and must be reviewed every five years and if not revised, either reapproved or withdrawn. Your comments are invited either for revision of this standard or for additional standards and should be addressed to ASTM International Headquarters. Your comments will receive careful consideration at a meeting of the responsible technical committee, which you may attend. If you feel that your comments have not received a fair hearing you should make your views known to the ASTM Committee on Standards, at the address shown below.

This standard is copyrighted by ASTM International, 100 Barr Harbor Drive, PO Box C700, West Conshohocken, PA 19428-2959, United States. Individual reprints (single or multiple copies) of this standard may be obtained by contacting ASTM at the above address or at 610-832-9585 (phone), 610-832-9555 (fax), or service@astm.org (e-mail); or through the ASTM website (www.astm.org).